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# Engineering of *Corynebacterium glutamicum* for growth and production of L-ornithine, L-lysine, and lycopene from hexuronic acids

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## Abstract

**Background:** Second-generation feedstocks such as lignocellulosic hydrolysates are more and more in the focus of sustainable biotechnological processes. *Corynebacterium glutamicum*, which is used in industrial amino acid production at a million-ton scale, has been engineered towards utilization of alternative carbon sources. As for other microorganisms, the focus has been set on the pentose sugars present in lignocellulosic hydrolysates. Utilization of the hexuronic acids D-galacturonic acid (abundant in pectin-rich waste streams such as peels and pulps) and D-glucuronic acid (a component of the side-chains of plant xylans) for growth and production with *C. glutamicum* has not yet been studied.

**Results:** Neither aldohexuronic acid supported growth of *C. glutamicum* as sole or combined carbon source, although its genome encodes a putative uronate isomerase sharing 28% identical amino acids with UxaC from *Escherichia coli*. Heterologous expression of the genes for both uptake and catabolism of D-galacturonic acid and D-glucuronic acid was required to enable growth of *C. glutamicum* with either aldohexuronic acid as the sole carbon source. When present in mixtures with glucose, the recombinant *C. glutamicum* strains co-utilized D-galacturonate with glucose and D-glucuronate with glucose, respectively. When transformed with the plasmid for uptake and catabolism of the aldohexuronates, model producer strains were able to grow with and produce from D-galacturonate or D-glucuronate as sole carbon source.

**Conclusions:** An easily transferable metabolic engineering strategy for access of *C. glutamicum* to aldohexuronates was developed and applied to growth and production of the amino acids L-lysine and L-ornithine as well as the terpene lycopene from D-galacturonate or D-glucuronate.

## Background

*Corynebacterium glutamicum* is a rod-shaped Gram-positive aerobic bacterium, which can be found in soil, sewages, vegetables, and fruits [1]. This bacterium is capable of utilizing various sugars as well as organic acids [2]. Among others, *C. glutamicum* has the ability to metabolize glucose, fructose, and sucrose as well as lactate, pyruvate, and acetate [2-4]. Characteristic of *C. glutamicum* is the capability of growing on mixtures of different carbon sources with a monoauxic growth [5,6] as opposed to diauxic growth observed for many other microorganisms such as *Escherichia coli* and *Bacillus subtilis* [7]. Only a few exceptions have been reported as

in the case of glucose-ethanol or acetate-ethanol mixtures, where preferential substrate utilization was observed [8].

Since its discovery, *C. glutamicum* has become an indispensable microorganism for the biotechnological industry [9]. From its initial use as a natural L-glutamate producer [10], it is currently used for production of other amino acids such as L-lysine, L-ornithine, L-methionine, and L-aspartate [11-14]. However, its importance has further increased as it was for production of non-natural products [9] such as isobutanol [15], ethanol [16], putrescine [14,17,18], cadaverine [19], carotenoids and terpenoids [20-25], and xylitol [26].

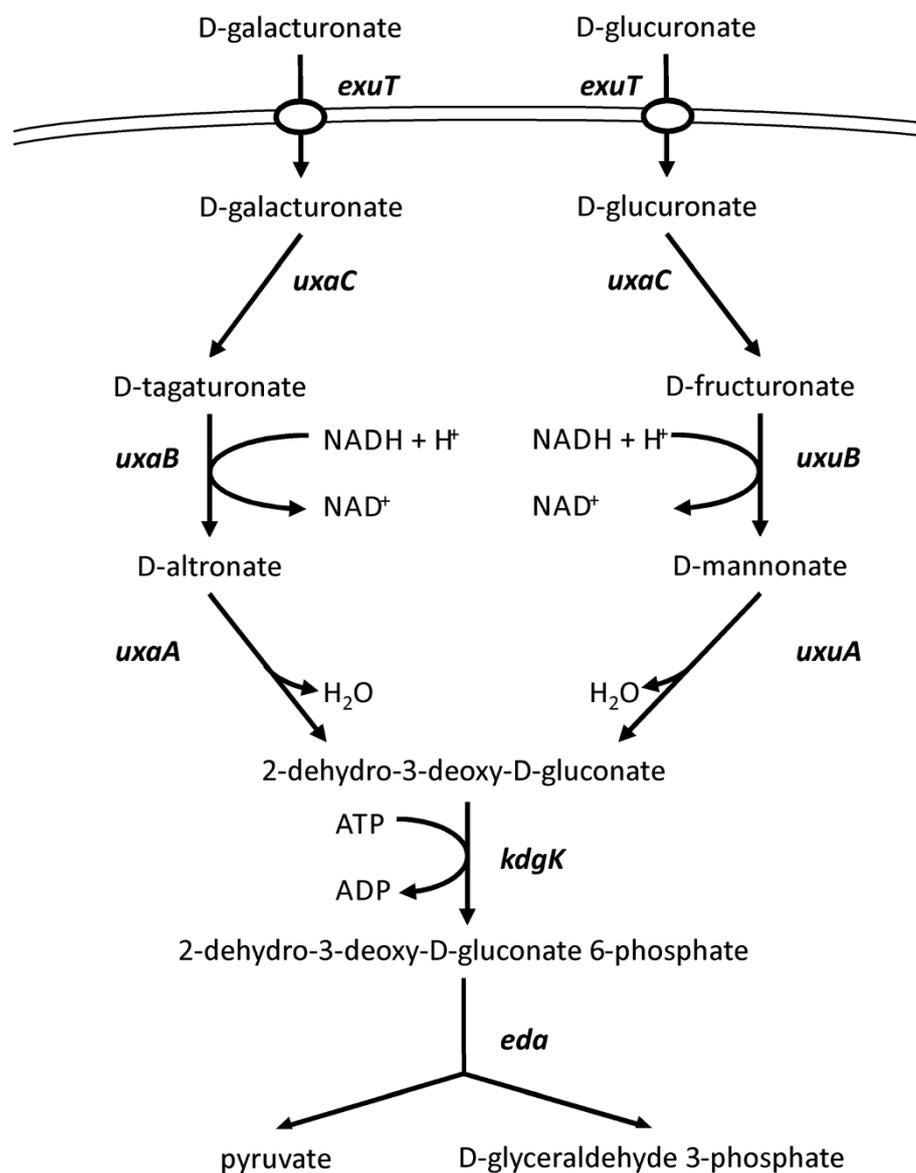
Recently, efforts with *C. glutamicum* have shifted from optimizing production processes to also include access to alternative carbon sources. As yet, feed in the industry

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relies mainly on glucose and fructose [8], which also have competing uses in the food industry. So far, alternative carbon source utilization in *C. glutamicum* has been successfully established, among others, for xylose [27,28], galactose [29], arabinose [14,30], glucosamine [31], N-acetyl-glucosamine [32], and glycerol [33]. Plant cell wall materials such as lignocellulose and pectin are promising alternatives as carbon source. These materials are readily and abundantly available as agricultural waste or forestry residues [34]. Among the sugar constituents of plant cell wall are the hexuronic acids D-galacturonate and D-

glucuronate found in pectin. These acidic sugars are naturally consumed by most plant pathogenic bacteria such as *Erwinia carotovora*, *Pseudomonas syringae*, and *Agrobacterium tumefaciens*, but also by *E. coli*.

There are three pathways for utilization of hexuronic acids, namely via isomerization, oxidation, and reduction [35]. The isomerization pathway in *E. coli* consists of seven reactions, which yield the central intermediates D-glyceraldehyde-3-phosphate and pyruvate (Figure 1). Both *uxaC-uxaA* and *uxuA-uxuB* are located within operons. However, these operons and the remaining genes



**Figure 1** Schematic representation of the D-galacturonate and D-glucuronate catabolic pathways of *E. coli*. Gene names are given adjacent to the reactions: *eda*, 2-keto-3-deoxygluconate-6-phosphate aldolase; *exuT*, uptake system for hexuronic acids; *kdgK*, 2-keto-3-deoxygluconokinase; *uxaA*, altronate dehydratase; *uxaB*, altronate oxidoreductase; *uxaC*, uronate isomerase; *uxuA*, mannonate dehydratase; *uxuB*, mannonate oxidoreductase.

are not clustered but spread across the genome of *E. coli*. The genes *kdgK* and *eda* belong to the modified Entner-Doudoroff pathway, which is present in many Gram-negative bacteria, pseudomonads, and Archaea [36]. Bioinformatic analysis revealed an *uxaC* ortholog in the genome of *C. glutamicum* with 28% protein similarity to that of *E. coli*. However, homologs of *uxaB*, *uxuA*, *uxuB*, *kdgK*, and *eda* appear to be absent. Therefore, in this work, *C. glutamicum* was engineered for the uptake and utilization of D-galacturonate and D-glucuronate as alternative carbon sources. The potential of this synthetic pathway was then analyzed with respect to the production of the amino acids L-lysine and L-ornithine as well as the carotenoid lycopene.

## Methods

### Microorganisms, plasmids, and cultivation conditions

The wild-type strain *C. glutamicum* ATCC 13032 used in this study was obtained from the American Type Culture Collection (ATCC). Other strains include *C. glutamicum* ORN1 [14], *C. glutamicum* DM1933 [37], and *C. glutamicum*  $\Delta$ *crtYEB* [23] that are derived from the wild-type strain (Table 1). The hexuronic acid utilization and transporter genes originated from *E. coli* MG1655, whereas the strain *E. coli* DH5 $\alpha$  [38] was used for plasmid construction. Both *E. coli* strains were obtained from the Coli Genetic Stock Center (CGSC). For cultivations, the Luria broth (LB) complex medium and CGXII minimal medium [39] were used and contained glucose,

**Table 1 Strains, plasmids, and oligonucleotides used in this study**

Name	Relevant genotype/information	Reference
<b><i>E. coli</i> strain</b>		
DH5 $\alpha$	( $\phi$ 80 <i>lacZ</i> $\Delta$ M15) $\Delta$ ( <i>lacZ</i> YA- <i>argF</i> )U169 <i>deoR recA1 endA1 hsdR17</i> ( <i>rK</i> -, <i>mK</i> -) <i>supE44 thi1 gyrA96 relA1</i>	[38]
<b><i>C. glutamicum</i> strains</b>		
WT	Wild-type strain ATCC 13032, auxotrophic for biotin	[40]
ORN1	In-frame deletion of <i>argR</i> and <i>argF</i> , L-ornithine overproducing strain derived from <i>C. glutamicum</i> WT ATCC 13032, auxotrophic for L-arginine	[14]
DM1933	$\Delta$ <i>pck</i> deletion mutant of <i>C. glutamicum</i> WT also carrying the chromosomal changes <i>pyc</i> (P458S), <i>hom</i> (V59A), two copies of <i>lysC</i> (T311), two copies of <i>asd</i> , two copies of <i>dapA</i> , two copies of <i>dapB</i> , two copies of <i>ddh</i> , two copies of <i>lysA</i> , two copies of <i>lysE</i>	[37]
$\Delta$ <i>crtYEB</i>	<i>crtY<sub>e</sub>Y<sub>f</sub>E<sub>b</sub></i> deletion mutant of <i>C. glutamicum</i> MB001	[23]
<b>Plasmids</b>		
pEKEx3	Spec <sup>R</sup> ; <i>E. coli</i> / <i>C. glutamicum</i> shuttle vector for regulated gene expression (P <sub>lac</sub> , <i>lacI<sup>f</sup></i> , pBL1 <i>oriV<sub>CG</sub></i> )	[41]
pHexA	pEKEx3 derivative for IPTG-inducible expression of <i>uxaCAB</i> , <i>uxuAB</i> , <i>kdgK</i> , and <i>eda</i> from <i>E. coli</i> containing artificial ribosome binding sites each	This work
pVWEx1	Km <sup>R</sup> ; <i>E. coli</i> / <i>C. glutamicum</i> shuttle vector for regulated gene expression (P <sub>lac</sub> , <i>lacI<sup>f</sup></i> , pCG1 <i>oriV<sub>CG</sub></i> )	[42]
pVWEx1- <i>exuT</i>	pVWEx1 derivative for IPTG-inducible expression of <i>exuT</i> from <i>E. coli</i> containing artificial ribosome binding site	This work
<b>Primers</b>		
G1a	GCAGGTCGACTCTAGAGGATCCCCGAAAGGAGGCCCTTCAGATGACTCCGTTTATGACTGAAGATTTTC	
G1b	GTAAGTCTAATGCAATCAGTGATGTTATAGCGTTACGCCGCTTTTG	
G2d	CATCACTGATTGCATTAGCTAGTACGAAAGGAGGCCCTTCAGATGAAAACTAAATCGTCGCGAT	
G2c	GCTAATGGTGCTATCTGGTACGATCTTAGCACAACGGACGTACAG	
G3d	GATCGTACCAGATAGCACCATAGCGAAAGGAGGCCCTTCAGATGGAACAGACCTGGGCC	
G3f	GCAGGTCGACTCTAGAGGATCCCCATGGAACAGACCTGGCGCTGGTACGGCC	
G3c	CGTTCTAGTTACTTTGGAACGTACCTTACAGCGCAGCCACACA	
G4d	GGTACGTTCCAAAGTAACTAGAACGAAAGGAGGCCCTTCAGATGTCCAAAAAGATTGCCGTGAT	
G4c	GTCAATCCATGGCATTCTAGCCAAGTTACGCTGGCATCGCCTC	
G5d	CTTGGCTAGAATGCCATGGATTGACGAAAGGAGGCCCTTCAGATGAAAACTGGAAAACAAGTGCAG	
G5c	GCCAGTGAATTCGAGCTCGGTACCTTACAGCTTAGCGCCTTCTACAG	
ExuT-fw	CTGCAGGTCGACTCTAGAGGAAAGGAGGCCCTTCAGA	
ExuT-rv	CGGTACCCGGGATCTTAATGTTGCGGTGCGGGATC	

D-galacturonate, or D-glucuronate in concentrations as indicated in the 'Results' section. Kanamycin (25  $\mu\text{g ml}^{-1}$ ), spectinomycin (100  $\mu\text{g ml}^{-1}$ ), and/or isopropyl- $\beta$ -D-thiogalactopyranoside (IPTG; 20  $\mu\text{M}$ ) were added to the medium when necessary. Cultivations were carried out in 50-ml cultures in 500-ml baffled Erlenmeyer flasks on a rotary shaker at 120 rpm and 30°C for *C. glutamicum* or 37°C for *E. coli*. In both cases, the growth in liquid cultures was followed by measuring the optical density at 600 nm ( $\text{OD}_{600}$ ).

#### DNA preparation, modification, and transformation

Standard procedures were used for plasmid and chromosomal DNA isolation, molecular cloning, and transformation of *E. coli*. Plasmid isolation for *C. glutamicum* was carried out as described previously [43]. Transformation of *C. glutamicum* by electroporation was carried out as described [39]. PCR experiments were carried out in a thermocycler (Analytik Jena AG, Jena, Germany) with KOD Hot Start DNA Polymerase (Novagen, Merck KGaA, Darmstadt, Germany) and with oligonucleotides obtained from Eurofins MWG Operon (Eurofins Genomics, Ebersberg, Germany) as listed in Table 2. Restriction enzymes, T4 DNA Ligase, and alkaline phosphatase were obtained from New England BioLabs, Inc. (Ipswich, MA, USA) and used according to the manufacturer's protocol.

#### Construction of plasmids and strains

For the construction of pHexA, the *uxaCA* and *uxuAB* operons as well as genes *uxaB*, *kdgK*, and *eda* were amplified by PCR from *E. coli* MG1655. The *uxaCA* operon was amplified with primers G1a + G1b resulting in a 2,981-bp product, whereas the *uxuAB* operon was amplified with primers G3f + G3c resulting in a 2,775-bp product. Gene *uxaB* was amplified with primers G2d + G2c, gene *kdgK* with primers G4d + G4c, and *eda* was amplified with primers G5d + G5c resulting in 1,519-, 997-, and 709-bp PCR products, respectively. Through these primers, appropriate linker sequences and a ribosomal binding site (RBS) sequence were attached to each gene or operon to facilitate the Gibson assembly [44]. The genetic load was first divided due to the insert size. Therefore, genes *uxuAB*, *kdgK*, and *eda* were cloned into the *SmaI*-digested pEKEx3 resulting in pEKEx3-*uxuAB-kdgK-eda*, designated as pAB5. The insert of pAB5 was amplified via PCR with primers G3d and G5d with a 4481-bp PCR product. The pAB5 amplicon, *uxaB*, and *uxaCA* were then used for Gibson assembly into the *SmaI*-digested pEKEx3 and yielded the final vector pHexA. The aldohexuronate transporter gene *exuT* was amplified via PCR with primers ExuT-fw and ExuT-rv from *E. coli* MG1655 and used for Gibson assembly into the BamHI-digested pVWEx1. The plasmid inserts were verified by sequencing (Sequencing Core Facility CeBiTec, Bielefeld,

Germany), and the plasmids were used to transform *C. glutamicum* ATCC 13032.

#### DNA microarray analysis

*C. glutamicum* ATCC 13032 was cultivated in CGXII medium with 50 mM D-galacturonate plus 50 mM glucose, 50 mM D-glucuronate plus 50 mM glucose, or 50 mM glucose as carbon source. Exponentially growing cells were harvested after 4 h. RNA isolation, cDNA synthesis, and microarray hybridization were performed according to previous protocols [45]. Microarray images were analyzed with ImaGene software (BioDiscovery, Inc., Hawthorne, CA, USA), whereas the EMMA platform was used for data evaluation.

#### Quantification of amino acids and carbohydrates

To evaluate the amino acid and carbohydrate production, culture samples were taken and centrifuged (13,000 $\times$ g, 10 min), and the supernatant analyzed by high-pressure liquid chromatography (HPLC, 1200 series, Agilent Technologies Inc., Santa Clara, CA, USA) as described previously [14,21].

#### Computational analysis

Protein alignments were carried out via the BLASTP algorithm [46] of NCBI (Bethesda, MD, USA). The GenBank accession number for the annotated genome sequence of *C. glutamicum* ATCC 13032 and *E. coli* MG1655 is NC\_006958 [47] and NC\_000913 [48], respectively.

## Results

#### Response of *C. glutamicum* WT to D-galacturonate and D-glucuronate

D-galacturonate and D-glucuronate were tested as potential carbon sources of *C. glutamicum*. However, although its genome encodes a putative uronate isomerase sharing 28% identical amino acids with UxaC from *E. coli*, both compounds did not support growth as sole carbon sources at 50 mM (data not shown). When present in addition to 50 mM glucose, *C. glutamicum* wild type (WT) grew to comparable maximal  $\text{OD}_{600}$  values of about 18 irrespective of the presence or absence of D-galacturonate or D-glucuronate (data not shown). Surprisingly, the presence of 50 mM D-galacturonate in minimal medium with 50 mM glucose accelerated growth slightly (0.24  $\text{h}^{-1}$  as compared to 0.17  $\text{h}^{-1}$ ), while the addition of 50 mM D-glucuronate to glucose minimal medium slowed growth of WT (0.13  $\text{h}^{-1}$ ). These observations prompted us to carry out DNA microarray experiments to study global gene expression under these conditions. Genes differentially expressed in cells growing exponentially with 50 mM D-galacturonate plus 50 mM glucose, 50 mM D-glucuronate plus 50 mM glucose, and 50 mM glucose alone are listed in Table 2. As expected, the presence of

**Table 2 Gene expression analysis of *C. glutamicum* WT in CGXII minimal medium with 50 mM glucose<sup>a</sup>**

	Gene ID	Description	M	
Differentially expressed genes in the presence of D-glucuronate	<i>cg3219</i>	<i>ldh</i> , L-lactate dehydrogenase	1.7	
	<i>cg3303</i>	Transcriptional regulator PadR family	1.6	
	<i>cg0580</i>	Hypothetical protein	1.5	
	<i>cg2789</i>	<i>nrhH</i> , glutaredoxin-like protein NrdH	-1.5	
	<i>cg2182</i>	ABC-type peptide transport system, permease component	-1.5	
	<i>cg3300</i>	Cation transport ATPase	-1.5	
	<i>cg2477</i>	Hypothetical protein	-1.6	
	<i>cg1809</i>	DNA-directed RNA polymerase subunit omega	-1.7	
	<i>cg0935</i>	Hypothetical protein	-1.8	
	<i>cg1286</i>	Hypothetical protein	-1.8	
	Differentially expressed genes in the presence of D-galacturonate	<i>cg2313</i>	<i>idhA3</i> , myo-inositol 2-dehydrogenase	2.0
		<i>cg1118</i>	Pyrimidine reductase, riboflavin biosynthesis	1.9
		<i>cg0687</i>	<i>gcp</i> , putative O-sialoglycoprotein endopeptidase	1.9
		<i>cg1116</i>	<i>tdcB</i> , threonine dehydratase	1.9
<i>cg1784</i>		<i>ocd</i> , putative ornithine cyclodeaminase	1.9	
<i>cg3096</i>		<i>ald</i> , aldehyde dehydrogenase	1.9	
<i>cg0792</i>		Thioredoxin domain-containing protein	1.8	
<i>cg0682</i>		ATPase or kinase	1.7	
<i>cg1003</i>		<i>ftnC</i> , 5-formyltetrahydrofolate cycloligase	1.7	
<i>cg1134</i>		<i>pabAB</i> , para-aminobenzoate synthase components I and II	1.7	
<i>cg1438</i>		ABC-type transport system, ATPase component (C-terminal fragment)	1.7	
<i>cg2430</i>		Hypothetical protein	1.7	
<i>cg1560</i>		<i>uvrA</i> , excinuclease ATPase subunit	1.7	
<i>cg1014</i>		<i>pmt</i> , protein O-mannosyltransferase	1.6	
<i>cg1668</i>		Putative membrane protein	1.6	
<i>cg2625</i>		<i>pcaF</i> , $\beta$ -ketoacyl CoA thiolase	1.6	
<i>cg2094</i>		Hypothetical protein	1.6	
<i>cg1241</i>		Hypothetical protein	1.5	
<i>cg1876</i>		Glycosyltransferase	1.5	

**Table 2 Gene expression analysis of *C. glutamicum* WT in CGXII minimal medium with 50 mM glucose<sup>a</sup> (Continued)**

<i>cg2417</i>	Short-chain-type oxidoreductase	1.5
<i>cg3118</i>	<i>cysI</i> , ferredoxin-sulfite reductase	-1.5
<i>cg0504</i>	<i>qsuD</i> , shikimate 5-dehydrogenase	-1.5
<i>cg1740</i>	Putative nucleoside-diphosphate-sugar epimerase	-1.5
<i>cg3225</i>	Putative serine/threonine-specific protein phosphatase	-1.5
<i>cg2945</i>	<i>ispD</i> , 2-C-methyl-D-erythritol 4-phosphate cytidyltransferase	-1.5
<i>cg1614</i>	Hypothetical protein	-1.5
<i>cg3427</i>	<i>parA1</i> , ATPase involved in chromosome partitioning	-1.5
<i>cg1252</i>	<i>fdxC</i> , ferredoxin	-1.5
<i>cg0518</i>	<i>hemL</i> , glutamate-1-semialdehyde 2,1-aminomutase	-1.5
<i>cg2587</i>	Phosphoglycerate dehydrogenase or related dehydrogenase	-1.6
<i>cg1551</i>	<i>uspA1</i> , universal stress protein UspA	-1.6
<i>cg0059</i>	<i>pknA</i> , serine/threonine protein kinase	-1.7
<i>cg0156</i>	<i>cysR</i> , transcriptional activator of assimilatory sulfate reduction	-1.7
<i>cg0966</i>	<i>thyA</i> , thymidylate synthase	-1.7
<i>cg0060</i>	<i>pbpA</i> , D-alanyl-D-alanine carboxypeptidase	-1.7
<i>cg1045</i>	Hypothetical protein	-1.7
<i>cg3119</i>	<i>fpr2</i> , probable sulfite reductase (flavoprotein)	-1.8
<i>cg1253</i>	Succinylidiaminopimelate aminotransferase	-1.8
<i>cg0045</i>	Putative ABC-type transporter membrane protein	-1.8
<i>cg3117</i>	<i>cysX</i> , ferredoxin-like protein	-1.8
<i>cg3430</i>	Hypothetical protein	-1.9
<i>cg3115</i>	<i>cysD</i> , sulfate adenyltransferase subunit 2	-1.9
<i>cg1037</i>	<i>rpf2</i> , RPF2 precursor	-1.9

<sup>a</sup>Statistical evaluation was carried out with the t-test, where  $p \leq 0.05$ , log expression ratio  $M \geq 1.5$  or  $\leq -1.5$ , and signal intensity  $A \geq 10$ . Values are averages of three independent cultivations.

D-galacturonate elicited different gene expression changes than D-glucuronate. Since neither D-galacturonate nor D-glucuronate was metabolized, these gene expression changes are likely due to regulatory or secondary effects. To elicit such regulatory changes, transport of minute

amounts of D-galacturonic or D-glucuronic acid might be sufficient.

Increased expression of fermentative lactate dehydrogenase gene *ldhA* in the presence of D-glucuronate might have slowed growth with glucose since lactate is known to accumulate transiently and since high *ldhA* levels have been implied to slow growth of *C. glutamicum* with sugars [49]. Furthermore, expression of the gene for subunit omega of RNA polymerase was reduced, thus transcription might have been negatively affected more in general. The gene expression changes due to the presence of D-galacturonate did not allow deriving a potential explanation for faster growth with glucose. However, decreased expression of *cg1551* encoding putative universal stress protein UspA is in line with faster growth of *C. glutamicum* in the presence of D-galacturonate.

#### Expression of genes for catabolism of D-galacturonate and D-glucuronate in *C. glutamicum* WT

Plasmid pHexA was constructed for heterologous expression of the *E. coli* genes for degradation of D-galacturonate and D-glucuronate to the glycolytic intermediates pyruvate and glyceraldehyde-3-phosphate. To this end, the operons *uxaCA* and *uxuAB* as well as genes *uxaB*, *kdgK*, and *eda* were cloned with attached RBS sequences as synthetic operon into IPTG-inducible gene expression vector pEKEx3. The resulting plasmid pHexA was used to transform *C. glutamicum* WT. However, the transformants were unable to grow with either D-galacturonate or D-glucuronate as sole carbon sources (data not shown).

#### Co-expression of *exuT* from *E. coli* was required for uptake of hexuronic acids

Since endowing *C. glutamicum* with D-galacturonate or D-glucuronate catabolism proved insufficient for utilization of these substrates, the gene for the respective uptake system *exuT* was co-expressed from a compatible plasmid. In preliminary experiments, *C. glutamicum* WT (pHexA)(pVWEx1-*exuT*) did indeed grow with either D-galacturonate or D-glucuronate as sole carbon source, however, very slowly. Based on the assumption that overproduction of transmembrane protein ExuT perturbed growth, the concentration of the inducer IPTG was titrated. Moreover, it was required to pre-cultivate the strain in minimal medium with a mixture of 50 mM glucose and 50 mM of either D-galacturonate or D-glucuronate as carbon source. In the main culture with 50 mM of either D-galacturonate or D-glucuronate, no growth was observed for *C. glutamicum* WT(pHexA)(pVWEx1). By contrast, *C. glutamicum* WT(pHexA)(pVWEx1-*exuT*) was able to grow with D-galacturonate and D-glucuronate, respectively, with growth rates of  $0.06 \pm 0.01$  and  $0.05 \pm 0.01$  h<sup>-1</sup>, respectively (data not shown). Thus, these results revealed that *C. glutamicum* WT lacks the ability for uptake and

catabolism of hexuronic acids and that heterologous expression of the genes from *E. coli* for uptake and catabolism of hexuronic acids enabled access of *C. glutamicum* to D-galacturonate and D-glucuronate as growth substrates.

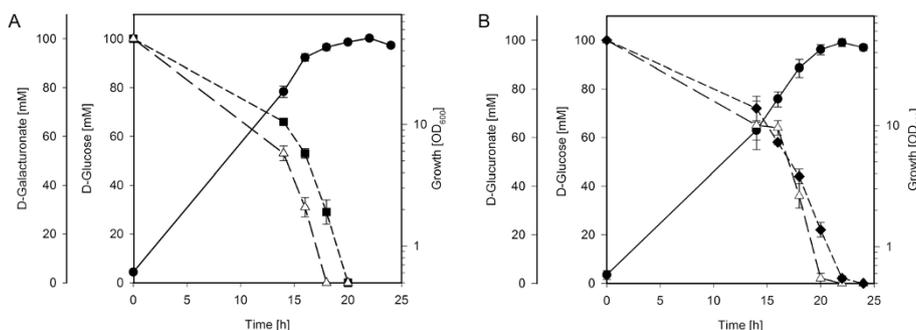
#### Co-utilization of hexuronic acids with glucose expression by *C. glutamicum* WT(pHexA)(pVWEx1)

A hallmark of *C. glutamicum* is its ability to co-utilize various carbon sources when these are added as carbon source mixtures. To assay if hexuronic acids are utilized simultaneously with glucose, the preferred carbon source of *C. glutamicum*, the growth and substrate consumption of *C. glutamicum* WT(pHexA)(pVWEx1) in minimal medium containing either 100 mM D-galacturonate plus 100 mM glucose or 100 mM D-glucuronate plus 100 mM glucose were determined (Figure 2). In minimal medium with the mixture of D-galacturonate plus glucose, *C. glutamicum* WT(pHexA)(pVWEx1) grew with a growth rate of  $0.25 \pm 0.02$  h<sup>-1</sup> and co-utilized glucose with D-galacturonate (Figure 2). Specific uptake rates of  $28 \pm 3$  and  $39 \pm 4$  nmol (mg cell dry weight (CDW))<sup>-1</sup> min<sup>-1</sup> were derived for utilization of D-galacturonate and glucose, respectively. In minimal medium with a blend of 100 mM D-glucuronate plus 100 mM glucose, both carbon sources were utilized simultaneously and support a growth rate of  $0.25 \pm 0.02$  h<sup>-1</sup> for *C. glutamicum* WT(pHexA)(pVWEx1) (Figure 2). The specific uptake rates were  $21 \pm 2$  nmol (mg CDW)<sup>-1</sup> min<sup>-1</sup> for glucose and  $18 \pm 2$  nmol (mg CDW)<sup>-1</sup> min<sup>-1</sup> for D-glucuronate.

#### Production of L-lysine, L-ornithine, and lycopene by recombinant *C. glutamicum* strains from D-galacturonate and D-glucuronate

The natural substrate spectrum of *C. glutamicum* has been broadened to realize a flexible feedstock concept for production processes using this bacterium [27-33]. To test if recombinant *C. glutamicum* strains engineered to accept D-galacturonate and D-glucuronate as growth substrates are able to produce, e.g., amino acids from these substrates, model L-lysine, L-ornithine, and lycopene producer strains were transformed with plasmids pHexA and pVWEx1-*exuT*. These strains were cultivated in CGXII minimal medium with 20 μM IPTG and either 100 mM D-galacturonate or 100 mM D-glucuronate as sole carbon source.

The lysine-producing strain *C. glutamicum* DM1933 carries a number of chromosomal changes known to be beneficial for L-lysine production [37]. DM1933(pHexA)(pVWEX1-*exuT*) hardly grew with either D-galacturonate or D-glucuronate (Table 3). However, DM1933(pHexA)(pVWEX1-*exuT*) produced  $6.5 \pm 0.2$  mM L-lysine from 100 mM D-galacturonate and  $9.3 \pm 1.1$  mM L-lysine from 100 mM D-glucuronate (Table 3).



**Figure 2** Growth of *C. glutamicum* strains WT(pHexA)(pVWEx1-exuT) with blends of D-glucose and D-galacturonate (A) or D-glucose and D-glucuronate (B). Residual concentrations of D-galacturonate (closed squares), D-glucuronate (closed diamonds), and D-glucose (open triangles) and OD600 values (closed circles) are given as means and standard deviations of triplicate cultivations in CGXII minimal medium, pH 6.3, with 20  $\mu$ M IPTG, and either a mixture of 100 mM D-galacturonate and 100 mM D-glucose (A) or a mixture of 100 mM D-glucuronate plus 100 mM D-glucose (B) as carbon sources.

Lycopene accumulates in *C. glutamicum*  $\Delta$ crtYEB due to disruption of the pathway for biosynthesis of the endogenous carotenoid decaprenoxanthin [20]. *C. glutamicum*  $\Delta$ crtYEB(pHexA)(pVWEX1-exuT) grew with D-galacturonate ( $0.02 \pm 0.01$  h<sup>-1</sup>) and D-glucuronate ( $0.04 \pm 0.01$  h<sup>-1</sup>), respectively, as sole carbon source (Table 3). The strain produced  $0.7 \pm 0.1$  mg (g CDW)<sup>-1</sup>

lycopene in minimal medium with D-galacturonate and  $0.8 \pm 0.3$  mg (g CDW)<sup>-1</sup> lycopene with D-glucuronate (Table 3).

**Table 3** Batch fermentations of L-lysine-, L-ornithine-, and lycopene-producing strains in minimal medium with D-galacturonate or D-glucuronate

	D-galacturonate	D-glucuronate
<b>L-lysine by DM1933(pHexA)(pVWEx1-exuT)</b>		
$C_{Lys}$ (mM)	$6.5 \pm 0.2$	$9.3 \pm 1.1$
$\mu$ (h <sup>-1</sup> )	$0.01 \pm 0.01$	$0.02 \pm 0.01$
$Y_{p/s}$ ( $g_{Lys} g_{substrate}^{-1}$ )	$0.04 \pm 0.01$	$0.07 \pm 0.01$
<b>Lycopene by <math>\Delta</math>crtYEB(pHexA)(pVWEx1-exuT)</b>		
$C_{Lyc}$ (mg/g)	$0.7 \pm 0.1$	$0.8 \pm 0.3$
$\mu$ (h <sup>-1</sup> )	$0.02 \pm 0.01$	$0.04 \pm 0.01$
$Y_{p/s}$ ( $g_{Lyc} g_{substrate}^{-1}$ )	$0.09 \pm 0.01$	$0.08 \pm 0.02$
<b>L-ornithine by ORN1(pHexA)(pVWEx1-exuT)</b>		
With 0.75 mM L-arginine		
$C_{Om}$ (mM)	$2.4 \pm 0.2$	<0.5
$\mu$ (h <sup>-1</sup> )	$0.03 \pm 0.01$	$0.03 \pm 0.01$
$Y_{p/s}$ ( $g_{Om} g_{substrate}^{-1}$ )	$0.01 \pm 0.01$	<0.01
With 0.125 mM L-arginine		
$C_{Om}$ (mM)	$1.7 \pm 0.1$	$0.6 \pm 0.2$
$\mu$ (h <sup>-1</sup> )	$0.04 \pm 0.01$	$0.03 \pm 0.01$
$Y_{p/s}$ ( $g_{Om} g_{substrate}^{-1}$ )	$0.01 \pm 0.01$	<0.01

CGXII minimal medium was used with 100 mM of the indicated carbon source.

*C. glutamicum* ORN1 is an L-arginine auxotrophic derivative of *C. glutamicum* WT that secretes L-ornithine due to deletions of the L-ornithine carbamoyltransferase gene *argF* and the L-arginine biosynthesis repressor gene *argR* [14]. When supplemented with either 0.75 mM or 0.125 mM L-arginine, *C. glutamicum* ORN1(pHexA)(pVWEX1-exuT) grew in D-galacturonate and D-glucuronate minimal medium with growth rates of about  $0.04 \pm 0.01$  h<sup>-1</sup> (Table 3). However, L-ornithine accumulated only to low concentrations corresponding to yields of about 1 to 2 mol% (Table 3).

## Discussion

*C. glutamicum* WT is not capable of utilizing hexuronic acids. Heterologous expression of gene for catabolism and uptake of the hexuronic acid pathway from *E. coli* in *C. glutamicum* enabled utilization of both D-galacturonate and D-glucuronate as sole carbon sources in minimal medium. Moreover, both hexuronates were co-utilized with glucose by the recombinant *C. glutamicum* strains developed here. Simultaneous utilization of several carbon sources as required for efficient utilization of substrate mixtures such as in lignocellulosic hydrolysates is a hallmark of *C. glutamicum* [6,8] and also pertains to co-utilization of non-native substrates by the respective recombinants [14,27,28,30-33].

Notably, the aldohexuronate transporter ExuT was strictly required, indicating that *C. glutamicum* lacks the capacity to import sugar acids. ExuT belongs to the major facilitator superfamily (MFS) class of transporters, more specifically to the anion:cation symporter (ACS) family [50]. This class of symporters transfers organic/inorganic anions while simultaneously co-transporting H<sup>+</sup>/Na<sup>+</sup>, respectively. ExuT has not been reported to transport other

substrates than the aldohexuronic acids. Inspection of the genome of *C. glutamicum* WT showed only one protein with 22% similarity to ExuT, namely putative lincomycin resistance protein LMRB (YP 226924.1). Engineering *C. glutamicum* for growth with other non-native carbon sources does not necessarily require heterologous expression of a gene encoding a transport system. Introduction of catabolic genes for conversion of glycerol, arabinose, and xylose was sufficient to enable utilization of these carbon sources by these recombinant *C. glutamicum* strains, while additional introduction of the respective uptake system accelerated carbon source utilization [27,28,33,51,52]. Transport engineering was not required for the amino sugar glucosamine, which is a substrate of the endogenous glucose-specific PTS [31], whereas the amino sugar N-acetylglucosamine could only be utilized if NagE from the related *Corynebacterium glycinophilum* was introduced [32]. In the latter case as well as in the present study, it was necessary to adjust the concentration of the inducer IPTG. It is often observed that too high levels of a transmembrane protein such as a transport protein results in growth perturbation [53,54]. In addition, expression levels of several genes of a pathway may need to be tuned to avoid accumulation of potentially inhibitory intermediates as demonstrated for *C. glutamicum* engineered for decaprenoxanthin overproduction [23].

It is not known if the recombinant *C. glutamicum* strain WT(pHexA)(pVWEX1-*exuT*) would be able to grow with sugar acids related to the aldohexuronates D-galacturonate and D-glucuronate since ExuT is specific for aldohexuronate uptake. In *E. coli*, the intermediate of aldohexuronate catabolism D-fructuronate serves as carbon source and its utilization requires uptake by GntP [55]. *C. glutamicum* possesses GntP for gluconate uptake [56], but it is unknown whether GntP from *C. glutamicum* accepts D-fructuronate or the related intermediates of aldohexuronate catabolism D-tagaturonate, D-altronate, or D-mannonate as substrates. Recently, it was shown that *E. coli* may grow with L-galactonate and L-gulonate as sole carbon sources with L-galactonate-5-dehydrogenase YjjN being required for their conversion to D-tagaturonate and D-fructuronate, respectively [57]. Under osmotic stress conditions, *E. coli* may use a different pathway, i.e., 5-keto 4-deoxyuronate isomerase KduI and 2-deoxy-D gluconate 3-dehydrogenase KduD may compensate for reduced levels of UxaC, UxaB, and UxuB under osmotic stress conditions [58]. Since ExuT from *E. coli* was required for aldohexuronate utilization by recombinant *C. glutamicum*, it is likely that introduction of the respective uptake systems for the related sugar acids described above is a prerequisite for their use as carbon sources.

Degradation of aldohexuronate to pyruvate yields one mole of ATP per mole of aldohexuronate by substrate-level phosphorylation as compared to two moles of ATP

per glucose in the Embden-Meyerhof-Parnas (EMP) pathway of glycolysis as present in *C. glutamicum*. In the EMP pathway of glycolysis, two moles of nicotinamide adenine dinucleotide (NADH) are generated from glucose, while no net formation of NADH occurs in aldohexuronate conversion to pyruvate (Figure 1). The maximal OD<sub>600</sub> values reflecting the maximal biomass concentration with 50 mM D-galacturonate consequently were lower (OD<sub>600</sub> of about 6.5) than with 50 mM glucose (OD<sub>600</sub> of about 18). The maximal OD<sub>600</sub> (about 4.5) with 50 mM D-glucuronate was even lower (data not shown). The reduced biomass yields for aerobic growth with the aldohexuronates can be explained at least in part by their lower ATP yields as compared to glucose catabolism. The growth rates in minimal medium with D-galacturonate (0.06 h<sup>-1</sup>) and D-glucuronate (0.05 h<sup>-1</sup>), respectively, obtained with *C. glutamicum* WT(pHexA)(pVWEX1-*exuT*) are five to six times lower than with glucose. Aldohexuronate utilization may be accelerated, e.g., by improving heterologous gene expression or by using catabolic enzymes of other microorganisms as in the case of xylose [28]. Instability of the plasmids pHexA and pVWEX1-*exuT* were not observed in the experiments described here; however, it might be possible that plasmid instability poses a challenge when using these strains in large fermentation vessels.

The low biomass yields and slow growth rates observed with *C. glutamicum* WT(pHexA)(pVWEX1-*exuT*) were also found when the respective plasmids were transformed into model producer strains. The product yields observed were low, e.g., about 6 to 9 mol% for L-lysine (Table 3). Thus, the aldohexuronates are not good substrates for growth and production by *C. glutamicum*. However, endowing *C. glutamicum* strains with aldohexuronate catabolism may be a requirement for complete and efficient utilization of second-generation feedstocks ensuring that not only the major sugar fractions are converted to value-added products.

## Conclusions

Access of *C. glutamicum* to the aldohexuronates D-galacturonate and D-glucuronate was established by heterologous expression of genes for catabolism and uptake of the aldohexuronates from *E. coli* in *C. glutamicum*. This metabolic engineering strategy could be applied to D-galacturonate- or D-glucuronate-based growth and production of the amino acids L-lysine and L-ornithine as well as the terpene lycopene.

## Competing interests

The authors declare that they have no competing interests.

## Authors' contributions

AH planned and performed the experiments, analyzed the data, and drafted the paper. IK performed the experiments and analyzed the data. SNL planned the experiments and analyzed the data. VFW designed and

coordinated the study, analyzed the data, and wrote the paper. All authors read and approved the final manuscript.

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#### References

- Eggeling L, Bott M (2005) Handbook of *Corynebacterium glutamicum*. CRC, Boca Raton
- Blombach B, Seibold GM (2010) Carbohydrate metabolism in *Corynebacterium glutamicum* and applications for the metabolic engineering of L-lysine production strains. *Appl Microbiol Biotechnol* 86(5):1313–1322, doi:10.1007/s00253-010-2537-z
- Cocaign M, Monnet C, Lindley ND (1993) Batch kinetics of *Corynebacterium glutamicum* during growth on various carbon sources: use of substrate mixtures to localise metabolic bottlenecks. *Appl Microbiol Biotechnol* 40:526–530
- Dominguez H, Cocaign-Bousquet M, Lindley ND (1997) Simultaneous consumption of glucose and fructose from sugar mixtures during batch growth of *Corynebacterium glutamicum*. *Appl Microbiol Biotechnol* 47(5):600–603
- Dominguez H, Nezondet C, Lindley ND, Cocaign M (1993) Modified carbon flux during oxygen limited growth of *Corynebacterium glutamicum* and the consequences for amino acid overproduction. *Biotech Lett* 15:449–454
- Wendisch VF, de Graaf AA, Sahn H, Eikmanns BJ (2000) Quantitative determination of metabolic fluxes during coutilization of two carbon sources: comparative analyses with *Corynebacterium glutamicum* during growth on acetate and/or glucose. *J Bacteriol* 182(11):3088–3096
- Monod J (1949) The growth of bacterial cultures. *Ann Rev Microbiol* 3:371–394
- Zahoor A, Lindner SN, Wendisch VF (2012) Metabolic engineering of *Corynebacterium glutamicum* aimed at alternative carbon sources and new products. *Comput Struct Biotechnol J* 3:e201210004, doi:10.5936/CSBJ.201210004
- Wendisch VF (2014) Microbial production of amino acids and derived chemicals: synthetic biology approaches to strain development. *Curr Opin Biotechnol* 30C:51–58, doi:10.1016/j.copbio.2014.05.004
- Ikeda M (2003) Amino acid production processes. *Adv Biochem Eng Biotechnol* 79:1–35
- Wendisch VF (2007) Amino acid biosynthesis – pathways, regulation and metabolic engineering. Springer, Heidelberg
- Hermann T (2003) Industrial production of amino acids by coryneform bacteria. *J Biotechnol* 104(1–3):155–172
- Leuchtenberger W, Huthmacher K, Drauz K (2005) Biotechnological production of amino acids and derivatives: current status and prospects. *Appl Microbiol Biotechnol* 69(1):1–8
- Schneider J, Niermann K, Wendisch VF (2011) Production of the amino acids L-glutamate, L-lysine, L-ornithine and L-arginine from arabinose by recombinant *Corynebacterium glutamicum*. *J Biotechnol* 154(2–3):191–198, doi:10.1016/j.jbiotec.2010.07.009
- Blombach B, Riestler T, Wieschalka S, Ziert C, Youn JW, Wendisch VF, Eikmanns BJ (2011) *Corynebacterium glutamicum* tailored for efficient isobutanol production. *Appl Environ Microbiol* 77(10):3300–3310, doi:10.1128/AEM.02972-10
- Inui M, Kawaguchi H, Murakami S, Vertes AA, Yukawa H (2004) Metabolic engineering of *Corynebacterium glutamicum* for fuel ethanol production under oxygen-deprivation conditions. *J Mol Microbiol Biotechnol* 8(4):243–254, doi:10.1159/000086705
- Schneider J, Wendisch VF (2010) Putrescine production by engineered *Corynebacterium glutamicum*. *Appl Microbiol Biotechnol* 88(4):859–868, doi:10.1007/s00253-010-2778-x
- Schneider J, Eberhardt D, Wendisch VF (2012) Improving putrescine production by *Corynebacterium glutamicum* by fine-tuning ornithine transcarbamoylase activity using a plasmid addition system. *Appl Microbiol Biotechnol* 95(1):169–178, doi:10.1007/s00253-012-3956-9
- Mimitsuka T, Sawai H, Hatsu M, Yamada K (2007) Metabolic engineering of *Corynebacterium glutamicum* for cadaverine fermentation. *Biosci Biotechnol Biochem* 71(9):2130–2135, doi:10.1271/bbb.60699
- Heider SA, Peters-Wendisch P, Netzer R, Stafnes M, Brautaset T, Wendisch VF (2014) Production and glucosylation of C50 and C 40 carotenoids by metabolically engineered *Corynebacterium glutamicum*. *Appl Microbiol Biotechnol* 98(3):1223–1235, doi:10.1007/s00253-013-5359-y
- Heider SA, Peters-Wendisch P, Wendisch VF (2012) Carotenoid biosynthesis and overproduction in *Corynebacterium glutamicum*. *BMC Microbiol* 12:198, doi:10.1186/1471-2180-12-198
- Heider SA, Peters-Wendisch P, Wendisch VF, Beekwilder J, Brautaset T (2014) Metabolic engineering for the microbial production of carotenoids and related products with a focus on the rare C50 carotenoids. *Appl Microbiol Biotechnol* 98(10):4355–4368, doi:10.1007/s00253-014-5693-8
- Heider SA, Wolf N, Hofemeier A, Peters-Wendisch P, Wendisch VF (2014) Optimization of the IPP precursor supply for the production of lycopene, decaprenoxanthin and astaxanthin by *Corynebacterium glutamicum*. *Front Bioeng Biotechnol* 2:28, doi:10.3389/fbioe.2014.00028
- Frohwitter J, Heider SA, Peters-Wendisch P, Beekwilder J, Wendisch VF (2014) Production of the sesquiterpene (+)-valencene by metabolically engineered *Corynebacterium glutamicum*. *J Biotechnol*, doi:10.1016/j.jbiotec.2014.05.032
- Kang MK, Eom JH, Kim Y, Um Y, Woo HM (2014) Biosynthesis of pinene from glucose using metabolically-engineered *Corynebacterium glutamicum*. *Biotechnol Lett* 36(10):2069–2077, doi:10.1007/s10529-014-1578-2
- Sasaki M, Jojima T, Inui M, Yukawa H (2009) Xylitol production by recombinant *Corynebacterium glutamicum* under oxygen deprivation. *Appl Microbiol Biotechnol* 86:1057–1066, doi:10.1007/s00253-009-2372-2
- Gopinath V, Meiswinkel TM, Wendisch VF, Nampoothiri KM (2011) Amino acid production from rice straw and wheat bran hydrolysates by recombinant pentose-utilizing *Corynebacterium glutamicum*. *Appl Microbiol Biotechnol* 92(5):985–996, doi:10.1007/s00253-011-3478-x
- Meiswinkel TM, Gopinath V, Lindner SN, Nampoothiri KM, Wendisch VF (2013) Accelerated pentose utilization by *Corynebacterium glutamicum* for accelerated production of lysine, glutamate, ornithine and putrescine. *Microb Biotechnol* 6(2):131–140, doi:10.1111/1751-7915.12001
- Barrett E, Stanton C, Zelder O, Fitzgerald G, Ross RP (2004) Heterologous expression of lactose- and galactose-utilizing pathways from lactic acid bacteria in *Corynebacterium glutamicum* for production of lysine in whey. *Appl Environ Microbiol* 70(5):2861–2866
- Kawaguchi H, Sasaki M, Vertes AA, Inui M, Yukawa H (2009) Identification and functional analysis of the gene cluster for L-arabinose utilization in *Corynebacterium glutamicum*. *Appl Environ Microbiol* 75(11):3419–3429, doi:10.1128/AEM.02912-08
- Uhde A, Youn JW, Maeda T, Clermont L, Matano C, Kramer R, Wendisch VF, Seibold GM, Marin K (2013) Glucosamine as carbon source for amino acid-producing *Corynebacterium glutamicum*. *Appl Microbiol Biotechnol* 97(4):1679–1687, doi:10.1007/s00253-012-4313-8
- Matano C, Uhde A, Youn JW, Maeda T, Clermont L, Marin K, Kramer R, Wendisch VF, Seibold GM (2014) Engineering of *Corynebacterium glutamicum* for growth and L-lysine and lycopene production from N-acetyl-glucosamine. *Appl Microbiol Biotechnol* 98(12):5633–5643, doi:10.1007/s00253-014-5676-9
- Rittmann D, Lindner SN, Wendisch VF (2008) Engineering of a glycerol utilization pathway for amino acid production by *Corynebacterium glutamicum*. *Appl Environ Microbiol* 74(20):6216–6222, doi:10.1128/AEM.00963-08
- Zaldivar J, Nielsen J, Olsson L (2001) Fuel ethanol production from lignocellulose: a challenge for metabolic engineering and process integration. *Appl Microbiol Biotechnol* 56(1–2):17–34
- Boer H, Maaheimo H, Koivula A, Penttila M, Richard P (2010) Identification in *Agrobacterium tumefaciens* of the D-galacturonic acid dehydrogenase gene. *Appl Microbiol Biotechnol* 86(3):901–909, doi:10.1007/s00253-009-2333-9
- Conway T (1992) The Entner-Doudoroff pathway: history, physiology and molecular biology. *FEMS Microbiol Rev* 9(1):1–27
- Blombach B, Hans S, Bathe B, Eikmanns BJ (2009) Acetohydroxyacid synthase, a novel target for improvement of L-lysine production by *Corynebacterium glutamicum*. *Appl Environ Microbiol* 75(2):419–427, doi:10.1128/AEM.01844-08
- Hanahan D (1983) Studies on transformation of *Escherichia coli* with plasmids. *J Mol Biol* 166(4):557–580
- Eggeling L, Reyes O (2005) Experiments. In: Eggeling L, Bott M (eds) Handbook of *Corynebacterium glutamicum*. CRC, Boca Raton, pp 3535–3566
- Abe S, Takayama K, Kinoshita S (1967) Taxonomical studies on glutamic acid-producing bacteria. *J Gen Appl Microbiol* 13:279–301

41. Stansen C, Uy D, Delaunay S, Eggeling L, Goergen JL, Wendisch VF (2005) Characterization of a *Corynebacterium glutamicum* lactate utilization operon induced during temperature-triggered glutamate production. *Appl Environ Microbiol* 71(10):5920–5928, doi:10.1128/AEM.71.10.5920-5928.2005
42. Peters-Wendisch PG, Schiel B, Wendisch VF, Katsoulidis E, Mockel B, Sahn H, Eikmanns BJ (2001) Pyruvate carboxylase is a major bottleneck for glutamate and lysine production by *Corynebacterium glutamicum*. *J Mol Microbiol Biotechnol* 3(2):295–300
43. Eikmanns BJ, Thum-Schmitz N, Eggeling L, Lüdtko KU, Sahn H (1994) Nucleotide sequence, expression and transcriptional analysis of the *Corynebacterium glutamicum* *glcA* gene encoding citrate synthase. *Microbiology* 140(Pt 8):1817–1828
44. Gibson DG, Young L, Chuang RY, Venter JC, Hutchison CA, 3rd, Smith HO (2009) Enzymatic assembly of DNA molecules up to several hundred kilobases. *Nat Methods* 6(5):343–345, doi:10.1038/nmeth.1318
45. Wendisch VF (2003) Genome-wide expression analysis in *Corynebacterium glutamicum* using DNA microarrays. *J Biotechnol* 104(1–3):273–285
46. Altschul SF1, Gish W, Miller W, Myers EW, Lipman DJ (1990) Basic local alignment search tool. *J Mol Biol* 215:403–410
47. Kalinowski J, Bathe B, Bartels D, Bischoff N, Bott M, Burkovski A, Dusch N, Eggeling L, Eikmanns BJ, Gaigalat L, Goesmann A, Hartmann M, Huthmacher K, Kramer R, Linke B, McHardy AC, Meyer F, Mockel B, Pfeifferle W, Puhler A, Rey DA, Ruckert C, Rupp O, Sahn H, Wendisch VF, Wiegrabe I, Tauch A (2003) The complete *Corynebacterium glutamicum* ATCC 13032 genome sequence and its impact on the production of L-aspartate-derived amino acids and vitamins. *J Biotechnol* 104(1–3):5–25
48. Blattner FR, Plunkett G 3rd, Bloch CA, Perna NT, Burland V, Riley M, Collado-Vides J, Glasner JD, Rode CK, Mayhew GF, Gregor J, Davis NW, Kirkpatrick HA, Goeden MA, Rose DJ, Mau B, Shao Y (1997) The complete genome sequence of *Escherichia coli* K-12. *Science* 277(5331):1453–1474
49. Engels V, Lindner SN, Wendisch VF (2008) The global repressor SugR controls expression of genes of glycolysis and of the L-lactate dehydrogenase LdhA in *Corynebacterium glutamicum*. *J Bacteriol* 190(24):8033–8044, doi:10.1128/JB.00705-08
50. Pao SS, Paulsen IT, Saier MH Jr (1998) Major facilitator superfamily. *Microbiol Mol Biol Rev* 62(1):1–34
51. Meiswinkel TM, Rittmann D, Lindner SN, Wendisch VF (2013) Crude glycerol-based production of amino acids and putrescine by *Corynebacterium glutamicum*. *Bioresour Technol* 145:254–258, doi:10.1016/j.biortech.2013.02.053
52. Sasaki M, Jojima T, Kawaguchi H, Inui M, Yukawa H (2009) Engineering of pentose transport in *Corynebacterium glutamicum* to improve simultaneous utilization of mixed sugars. *Appl Microbiol Biotechnol* 85(1):105–115, doi:10.1007/s00253-009-2065-x
53. Youn JW, Jolkver E, Kramer R, Marin K, Wendisch VF (2008) Identification and characterization of the dicarboxylate uptake system DccT in *Corynebacterium glutamicum*. *J Bacteriol* 190(19):6458–6466, doi:10.1128/JB.00780-08
54. Youn JW, Jolkver E, Kramer R, Marin K, Wendisch VF (2009) Characterization of the dicarboxylate transporter DctA in *Corynebacterium glutamicum*. *J Bacteriol* 191(17):5480–5488, doi:10.1128/JB.00640-09
55. Bates Utz C, Nguyen AB, Smalley DJ, Anderson AB, Conway T (2004) GntP is the *Escherichia coli* fructuronic acid transporter and belongs to the UxuR regulon. *J Bacteriol* 186(22):7690–7696, doi:10.1128/JB.186.22.7690-7696.2004
56. Frunzke J, Engels V, Hasenbein S, Gatgens C, Bott M (2008) Co-ordinated regulation of gluconate catabolism and glucose uptake in *Corynebacterium glutamicum* by two functionally equivalent transcriptional regulators, GntR1 and GntR2. *Mol Microbiol* 67(2):305–322, doi:10.1111/j.1365-2958.2007.06020.x
57. Kuivanen J, Richard P (2014) The *yjiN* of *E. coli* codes for an L-galactonate dehydrogenase and can be used for quantification of L-galactonate and L-gulonate. *Appl Biochem Biotechnol* 173(7):1829–1835, doi:10.1007/s12010-014-0969-0
58. Rothe M, Alpert C, Loh G, Blaut M (2013) Novel insights into *E. coli*'s hexuronate metabolism: Kdul facilitates the conversion of galacturonate and glucuronate under osmotic stress conditions. *PLoS One* 8(2):e56906, doi:10.1371/journal.pone.0056906

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