

REVIEW

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Progress and perspective on lignocellulosic hydrolysate inhibitor tolerance improvement in *Zymomonas mobilis*

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Abstract

Pretreatment is the key step to overcome the recalcitrance of lignocellulosic biomass making sugars available for subsequent enzymatic hydrolysis and microbial fermentation. During the process of pretreatment and enzymatic hydrolysis as well as fermentation, various toxic compounds may be generated with strong inhibition on cell growth and the metabolic capacity of fermenting strains. *Zymomonas mobilis* is a natural ethanologenic bacterium with many desirable industrial characteristics, but it can also be severely affected by lignocellulosic hydrolysate inhibitors. In this review, analytical methods to identify and quantify potential inhibitory compounds generated during lignocellulose pretreatment and enzymatic hydrolysis were discussed. The effect of hydrolysate inhibitors on *Z. mobilis* was also summarized as well as corresponding approaches especially the high-throughput ones for the evaluation. Then the strategies to enhance inhibitor tolerance of *Z. mobilis* were presented, which include both forward and reverse genetics approaches such as classical and novel mutagenesis approaches, adaptive laboratory evolution, as well as genetic and metabolic engineering. Moreover, this review provided perspectives and guidelines for future developments of robust strains for efficient bioethanol or biochemical production from lignocellulosic materials.

Keywords: Lignocellulose, Inhibitor, *Zymomonas mobilis*, Robustness, Adaptive laboratory evolution (ALE), Mutagenesis, Systems biology, Metabolic engineering

Background

Due to the exhaustibility of fossil fuels and its indiscriminate use, there is an urgent need for the development of sustainable and affordable alternatives. Lignocellulosic materials such as agriculture wastes, forestry residues, and energy plants are considered as an abundant and renewable feedstock for bioenergy production through biochemical conversion. However, these biomass resources are naturally recalcitrant that carbohydrates of cellulose and hemicellulose are closely associated with lignin in the plant cell wall. Pretreatment is required to breakdown the rigid cell wall structure and

to make polysaccharides available for subsequent enzymatic hydrolysis and fermentation. During the deconstruction processes, various inhibitory compounds with strong inhibition on cell growth and metabolic capacity of fermenting strains are generated due to the partial over-degradation of lignocellulose. The toxic nature of the lignocellulosic hydrolysate severely impedes its efficient substrate utilization and bioethanol fermentation. Although methods to remove inhibitors physically, chemically, or biologically may help moderate the problem of toxic compounds in lignocellulosic hydrolysates, it is not economically feasible to remove inhibitors from hydrolysate prior to fermentation due to the cost associated with additional processing steps and the potential loss of fermentable sugars (Jönsson et al. 2013; Parawira and Tekere 2011). Therefore, it is a key barrier to develop

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and employ robust inhibitor-tolerant microorganisms for economic lignocellulosic biofuel production.

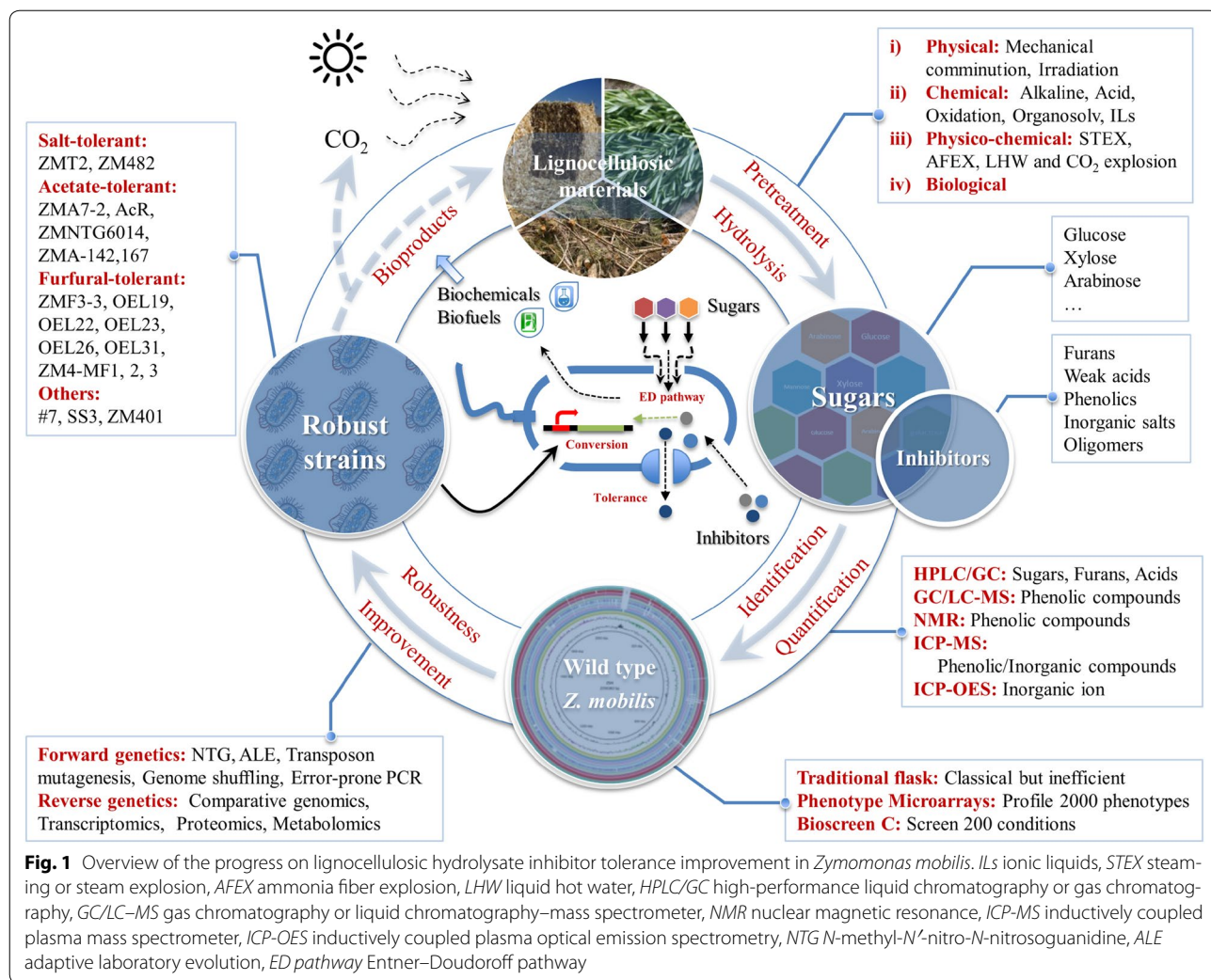
Several microorganisms have been applied for ethanol production from lignocellulose, including both bacteria and yeasts (Olsson and Hahn-Hägerdal 1996). As a model bioethanol producer, *Zymomonas mobilis* has attracted considerable attention over the past decades due to its excellent industrial characteristics, such as the unique Entner–Doudoroff (ED) pathway under anaerobic conditions resulting in low cell mass formation, high specific rate of sugar uptake, high ethanol yield, notable ethanol tolerance, and the generally regarded as safe (GRAS) status (Panesar et al. 2006; Rogers et al. 2007). Furthermore, the availability of multiple genome sequences for 12 *Zymomonas* strains with small genome size around 2 Mb (Seo et al. 2005; Yang et al. 2009a; Zhao et al. 2012), multiple genome-scale metabolic models (Kalnenieks et al. 2014; Pentjuss et al. 2013; Widiastuti et al. 2011), and versatile genetic engineering strategies (Jia et al. 2013; Shui et al. 2015; Tan et al. 2016) also accelerates the research progress in *Z. mobilis*. *Z. mobilis* has also been engineered for the production of sorbitol, gluconic acid, levan, 2,3-butanediol, isobutanol, and other biochemicals, which is proposed as an ideal microbial chassis for future synthetic biology and biorefinery (He et al. 2014; Yang et al. 2016).

Although *Z. mobilis* demonstrates advantages in ethanol fermentation, the inhibitors derived from biomass deconstruction and hydrolysis still have detrimental effects on *Z. mobilis*, especially when high biomass solid loading is used during pretreatment and enzymatic hydrolysis steps to generate high concentration of sugars besides the potential additive or synergistic inhibitions of various inhibitors in the hydrolysate (Fränden et al. 2013). In this review, we reviewed the progress of strain improvement in *Z. mobilis* to enhance its lignocellulosic hydrolysate inhibitor tolerance capability for economic lignocellulosic biochemical production. Specifically, strategies to identify and quantify potential inhibitory compounds generated during lignocellulose pretreatment and enzymatic hydrolysis were discussed. Different approaches especially the high-throughput ones to evaluate the inhibitory compounds on *Z. mobilis* were examined. Moreover, strategies of both forward and reverse genetics for inhibitor tolerance improvement in *Z. mobilis* were summarized. These strategies include classical and novel mutagenesis approaches, adaptive laboratory evolution (ALE), as well as genetic and metabolic engineering. We further proposed potential research directions to construct robust strains for bioethanol or biochemical production from lignocellulose feedstock in the synthetic biology era (Fig. 1).

Identification and quantification of inhibitors in lignocellulosic hydrolysate

Lignocellulose consists of three major polymerized components of cellulose, hemicellulose, and lignin, which are joined together with complex covalent bond, and difficult for microbial digestion (Sun and Cheng 2002). Owing to the recalcitrant structural characteristics of plant cell wall, pretreatment and enzymatic hydrolysis are the crucial steps to release mono-sugars from biomass for fermentation. The purpose of the pretreatment is to break down the lignin structure, disrupt the crystalline of cellulose, and increase the porosity of lignocellulose for enhancing enzymes accessibility to the cellulose during hydrolysis process. Various pretreatment approaches have been developed and examined. Generally, they can be classified into four categories: physical methods including mechanical comminution, extrusion, and irradiation; chemical methods including acid pretreatment (dilute acid or concentrated acid), alkaline pretreatment, oxidation, organosolv, and ionic liquids (ILs) pretreatment; physico-chemical methods including steaming or steam explosion (STEX), ammonia fiber explosion (AFEX), liquid hot water (LHW), and CO₂ explosion; and biological methods, which use microorganisms or enzymes to degrade lignocellulosic materials. Different pretreatment methods with regard to their features, advantages, and disadvantages as well as their impact on lignocellulosic materials have been discussed in detail in other reviews (Baral et al. 2014; Capolupo and Faraco 2016; Silveira et al. 2015; Sun et al. 2016). During the pretreatment process, a number of degradation products of lignin and sugar are generated, which could have detrimental effects on subsequent enzymatic hydrolysis and microbial cell fermentation (Jönsson et al. 2013).

Different biomass feedstock and pretreatment methods generate hydrolysates with distinctive toxic compounds, but three major groups of toxic compounds are usually classified in general. These are furan aldehydes, 2-furylaldehyde (furfural), and 5-hydroxymethyl-2-furaldehyde (HMF) produced by the dehydration of pentose and hexose sugars, respectively; weak organic acids, especially acetic acid produced by the deacetylation of hemicellulose and lignin, formic acid produced by the degradation of furans, and levulinic acid produced by the degradation of HMF; as well as phenolic compounds formed by the breakdown of lignin components (Almeida et al. 2007; Klinke et al. 2004). In addition to these three major components, a range of inorganic salts including alkali salts and heavy metal salts are present in lignocellulosic hydrolysates in varying degrees. Inorganic salts are different from all above three categories, since they are not generated from the over-degradation of lignocellulosic biomass, but from chemicals added during pretreatment



process or the corrosion of the walls of the pretreatment equipment (Klinke et al. 2004).

Many different kinds of analytical methods have been employed to identify and quantify compounds in the lignocellulosic hydrolysates. The major components of glucose, xylose, arabinose, acetic acid, and furans, as well as a wide variety of aliphatic acid compounds can be detected directly from hydrolysate samples by high-performance liquid chromatography (HPLC) or gas chromatography (GC) using different columns and detectors (Franden et al. 2013; Gu et al. 2014). Minor components, especially for phenolic compounds, have been extracted from hydrolysate using organic solvents, concentrated by evaporation, and analyzed by gas chromatography–mass spectrometer (GC–MS), liquid chromatography–mass spectrometer (LC–MS), and/or inductively coupled plasma mass spectrometer (ICP–MS) (Gu et al. 2014; Wang et al. 2014). Inductively coupled plasma optical

emission spectrometry (ICP–OES) has also been used for inorganic ion analysis and many different mineral elements such as magnesium, potassium, manganese, iron, copper, and calcium have been identified in lignocellulosic hydrolysates (Jin et al. 2013; Le et al. 2014). In addition, nuclear magnetic resonance (NMR) has been used recently as a nondestructive method for the structural investigation of lignocellulosic biomass at a molecular level during the deconstruction process which can contribute to the identification of new inhibitor compounds (Shi et al. 2011).

Evaluation of the effect of hydrolysate inhibitors on *Z. mobilis*

Fermentation performances of different microorganisms in lignocellulosic hydrolysates are distinctive, which are related to inhibitory compounds generated from diversified feedstock and pretreatment strategies. It is thus

critical to examine the toxic effect of hydrolysate compounds on cell growth and fermentation performance to help elucidate inhibitor tolerance mechanisms and to allow the development of robust industrial strains for economic biochemical production. Since cell growth is closely associated with ethanol production for many microorganisms including *Z. mobilis* (Delgenes et al. 1996; Zaldivar et al. 1999), it can provide relatively reliable estimates of the inhibitory effect of toxic compounds on microbial cells by measuring cell viability and growth with sensitive assays.

Traditional shake flask culture techniques for individual growth-associated assays are routinely used, but it is time-consuming, laborious, and inefficient. To solve the disadvantages of this classical method, various high-throughput evaluation techniques have been developed recently such as Biolog's Phenotype Microarrays, Bioscreen C, and BioLector. Phenotype Microarray system has been used to profile nearly 2000 *Z. mobilis* cellular phenotypes and provided an overview of *Z. mobilis* physiology (Bochner et al. 2010). In addition, a quantitative high-throughput biological growth assay based on turbidometric measurements using the Bioscreen C system was also established. This approach is capable of monitoring two 100-well plates at a 0.4-mL scale simultaneously, and has been widely used for cellular growth measurement in the presence of inhibitors and hydrolysate (Franden et al. 2009, 2013). It can provide detailed inhibitory kinetic data for individual inhibitory compounds in terms of continuing cellular growth and final cell mass.

Using conventional and high-throughput growth assays, effects of inhibitory hydrolysate compounds on *Z. mobilis* growth and fermentation have been investigated (Dong et al. 2013; Franden et al. 2009, 2013; Gu et al. 2015; Yi et al. 2015). The results demonstrated that acetate, furfural, and phenolic aldehydes are three major inhibitors in the dilute acid-pretreated corn stover hydrolysate for *Z. mobilis*, and the inhibitory activity was strongly correlated to the hydrophobicity of these compounds. Furthermore, combinations of HMF, furfural, and acetate resulted in additive rather than synergistic inhibition to *Z. mobilis* cell growth (Franden et al. 2013). It was also observed that *Z. mobilis* is capable of converting aldehydes of furfural, HMF, vanillin, 4-hydroxybenzaldehyde, and syringaldehyde to their corresponding alcohol forms of furfuryl, 5-hydroxymethylfurfural, vanillyl, 4-hydroxybenzyl, and syringyl alcohol, respectively (Franden et al. 2013; Yi et al. 2015). These studies suggested that the enhanced conversion of toxic aldehydes into the relatively benign alcohol forms with engineered strains could reduce process cost by improving ethanol yields and/or by reducing fermentation time.

Other than the inhibitory effects directly on cell growth, here, we also summarized the ethanol fermentation performances by *Z. mobilis* within lignocellulosic hydrolysates (Table 1). Compared with the results with pure sugars, ethanol productions in hydrolysates were impeded significantly (Bothast et al. 1999; Feng et al. 2012; Jennings and Schell 2011; Jeon et al. 2010; Joachimsthal et al. 1999; Krishnan et al. 2000; Mohagheghi et al. 2002, 2004; Schell et al. 2016; Serate et al. 2015; Teixeira et al. 2000; Yanase et al. 2012; Zhao et al. 2014). For example, the ethanol yield was much lower in the hydrolysate (15 g/L) than in pure glucose fermentation (44.9 g/L) (Dong et al. 2013; Zhao et al. 2014). These results showed that more efforts are needed to improve the inhibitor tolerance of *Z. mobilis*, especially in the hydrolysates where different inhibitors co-exist and with potential additive or synergistic effects.

Strategies to enhance inhibitor tolerance of *Z. mobilis*

To minimize the toxic effect of lignocellulosic hydrolysates on microbial fermentation and biofuel production, many efforts have been taken to screen and/or develop robust strains with improved tolerance toward these inhibitors. Recent studies showed that *Z. mobilis* biofilm cells exhibited a higher survival rate and metabolic activity than planktonic or free cells, which can also be developed and applied for the production of valuable bioproducts from toxic lignocellulosic hydrolysates (Li et al. 2006; Todhanakasem et al. 2014, 2015, 2018).

Many genetic approaches including forward and reverse genetics were applied to improve the innate inhibitor tolerance capability of *Z. mobilis* strains, and will be discussed below in detail (Table 2). Forward genetics approaches use ALE or mutagenesis approaches to generate and select mutants with desired phenotypes. Reverse genetics is an omics-guided systems metabolic engineering method to associate genetic candidates with desired phenotypes and then to transfer the genetic candidates into the host strains for robustness improvement.

Robustness improvement by forward genetics approaches

ALE is a powerful method to improve industrial features of microbial biocatalysts without a priori knowledge of any underlying genetic mechanisms (Portnoy et al. 2011), as long as the desired trait can be coupled with growth or other easily detectable phenotypes (Dragosits and Mattanovich 2013). ALE is still valuable for robustness improvement in *Z. mobilis*. *Z. mobilis* strains with increased tolerance toward furfural and acetic acid have been obtained by sequential transfers of cell cultures to synthetic media containing increasing concentrations of

Table 1 Ethanol fermentation by *Z. mobilis* in lignocellulosic hydrolysates compared to pure sugars

Carbon source	Pretreatment method	<i>Z. mobilis</i> strain	Fermentation	Sugar (g/L)	Inhibitors (g/L)	Ethanol titer (g/L)	References
Glucose		ZM4	Batch fermentation in 2.5-L bioreactor	100.0		44.9	Zhao et al. (2014)
Xylose		TSH-01	2-L bioreactor	80.0		> 30.0	Feng et al. (2012)
Glucose and xylose		ZM4 (pZB5)	Batch fermentation in 2-L fermentor	Glucose: 65.0 Xylose: 65.0		62.0	Joachimsthal et al. (1999)
Glucose, xylose, and mannose		<i>Z. mobilis</i> [sucZE2::manA, pZA22-xtR]	200-mL bioreactor	Glucose: 20.0 Xylose: 20.0 Mannose: 20.0		26.5	Yanase et al. (2012)
Glucose, xylose, and arabinose		AX101	BioStat-Q fermentors	Glucose: 40.0 Xylose: 40.0 Arabinose: 20.0		42.0	Mohagheghi et al. (2002)
Corn stover	DA	8b	500-mL bioreactor	Glucose: 14.5 Xylose: 90.9 Arabinose: 11.1 Galactose: 7.0	Acetic acid: 5.9 Furfural: 5.2 5-HMF: 0.2	> 60.0	Schell et al. (2016)
Corn stover	DA with NH ₄ OH-treated	8b	250-mL flasks	Glucose: 31.4 Xylose: 85.7 Fructose: 4.2 Arabinose: 11.2 Galactose: 6.6	Acetic acid: 16.3 HMF: 3.7 Furfural: 2.3	> 48.0 ^a	Jennings and Schell (2011)
Corn stover	DA	8b	BioStat-Q fermentors	Glucose: 16.0 Xylose: 69.0	Acetic acid: 11.0	36.6 ^b	Mohagheghi et al. (2004)
Corn stover	AFEX followed autoclaving	2302	500-mL bioreactor	Glucose: 63.9 Xylose: 31.7	Furfural: 6.5 5-HMF: 0.1 Vanillin: 21.5 Syringaldehyde: 1.3	39.1	Serate et al. (2015)
Switchgrass	AFEX followed autoclaving	2302	500-mL bioreactor	Glucose: 59.1 Xylose: 31.2	Furfural: 5.2 5-HMF: 0.1 Vanillin: 11.6 Syringaldehyde: 1.0	38.3	Serate et al. (2015)
Corn stover	DASE	ZM401	Batch fermentation in 2.5-L bioreactor	Glucose: 80.00 Xylose: 33.00	Furfural: 0.49 HMF: 0.28 Acetic acid: 0.66	> 27.5	Zhao et al. (2014)
Corn stover	DDAP	ZM4	3-L fermentor	Glucose: 58.36	Furfural: 0.26 HMF: 0.29 Formic acid: 0.92	15.0	Dong et al. (2013)
Corn stover	DA	TSH-01	2-L bioreactor	Glucose: 5.8 Xylose: 18.2 Arabinose: 1.1	Acetic acid: 7.5 Formic acid: 1.2 Furfural: 0.6	> 30.0	Feng et al. (2012)
Coniferous trees	DA	<i>Z. mobilis</i> [sucZE2::manA, pZA22-xtR]	Continuous fermentation Laboratory-scale bioreactor	Glucose: 68.5 Xylose: 14.3 Mannose: 22.4		37.3	Yanase et al. (2012)
Wheat straw	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 23.3 Xylose: 19 Arabinose: 3.0	Acetate: 3.1 Formate: 0.6 Levulinic acid: 0.7 HMF: 0.08 Furfural: 0.67	13.8	Jeon et al. (2010)
Bagasse	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 26.9 Xylose: 18.2 Arabinose: 2.8	Acetate: 4.1 Formate: 0.7 Levulinic acid: 0.8 HMF: 0.1 Furfural: 0.74	17.7	Jeon et al. (2010)

Table 1 continued

Carbon source	Pretreatment method	<i>Z. mobilis</i> strain	Fermentation	Sugar (g/L)	Inhibitors (g/L)	Ethanol titer (g/L)	References
Sorghum straw	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 22.0 Xylose: 16.9 Arabinose: 3.7	Acetate: 2.3 Formate: 1.2 Levulinic acid: 2.6 HMF: 0.6 Furfural: 0.5	10.6	Jeon et al. (2010)
Sugarcane tops	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 22.3 Xylose: 18.7 Arabinose: 3.1	Acetate: 2.1 Formate: 0.2 Levulinic acid: 0.2 HMF: 0.14 Furfural: 0.14	10.3	Jeon et al. (2010)
Arundo donax	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 17.7 Xylose: 23.3 Arabinose: 2.2	Acetate: 4.8 Formate: 0.5 Levulinic acid: 0.2 HMF: 0.04 Furfural: 0.74	12.3	Jeon et al. (2010)
Oil mallee	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 10.6 Xylose: 3.4 Arabinose: 5.0	Acetate: 0.7 Formate: 0.5 Levulinic acid: 0.7 HMF: 0.05 Furfural: 0.96	3.8	Jeon et al. (2010)
Pine	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 10.6 Xylose: 19.7 Arabinose: 1.5	Acetate: 1.8 Formate: 0.6 Levulinic acid: 0.4 HMF: 0.14 Furfural: 0.15	0.2	Jeon et al. (2010)
Eucalyptus	DA	ZM4 (pZB5)	Batch fermentation in 100-mL flasks	Glucose: 8.9 Xylose: 14.6 Arabinose: 0.3	Acetate: 3.4 Formate: 0.3 Levulinic acid: 0.2 Furfural: 0.2	2.3	Jeon et al. (2010)
Sugar cane bagasse	6% NaOH/15% peracetic acid	CP4 (pZB5)	SSCF in 250-mL flask			21.1	Teixeira et al. (2000)
Hybrid poplar wood	6% NaOH/15% peracetic acid	CP4 (pZB5)	SSCF in 250-mL flask			21.3	Teixeira et al. (2000)
Rice straw	Concentrated acid	CP4 (pZB5)	Batch fermentation in 125-mL flasks	Glucose: 76.0 Xylose: 33.8		44.3	Krishnan et al. (2000)
Corn fiber	DA	CP4 (pZB5)				22.6	Bothast et al. (1999)

DA dilute acid, DASE dilute acid steam explosion, STEX steaming or steam explosion, AFEX ammonia fiber explosion, DDAP dry dilute acid pretreatment, SSF simultaneous saccharification and fermentation, ASSF advanced solid-state fermentation technology, SSCF simultaneous saccharification and co-fermentation, 5-HMF 5-hydroxymethyl furfural

^{a, b} Ethanol titers in these two studies were calculated from the reported ethanol yield of 80%^a and 85%^b based on the maximum theoretical yield of total amount of glucose and xylose to ethanol

inhibitors (Shui et al. 2015). After three rounds of ALE, two selected mutants of ZMF3-3 and ZMA7-2 demonstrated higher growth capacity and faster glucose utilization than wild-type ZM4 under 3 g/L furfural or 7 g/L acetic acid stress conditions. A mutant strain #7 derived from *Z. mobilis* 8b was generated through adaptation with 5 g/L acetate, which had improved sugar utilization in the presence of inhibitory compounds of acetate

and furfural in the pretreated corn stover hydrolysates (Mohagheghi et al. 2014). Similarly, an adapted strain SS3 was selected after 70 days of continuous culturing using a turbidostatic with a gradually increasing concentration of the corn stover hydrolysate liquor, which had higher sugar utilization rate and ethanol productivity than that of parent strain *Z. mobilis* 8b in the corn stover hydrolysate (Mohagheghi et al. 2015).

Table 2 Tolerance improved strains obtained by forward genetics approaches

Parental strain	Technique(s)	Mutant(s)	Improved phenotype	References
ZM4	ALE	ZMF3-3	Cell growth, glucose utilization, and ethanol yield under 3 g/L furfural	Shui et al. (2015)
ZM4	ALE	ZMA7-2	Cell growth and glucose utilization under 7 g/L acetic acid	Shui et al. (2015)
8b	ALE	#7	Sugars utilization and ethanol production in corn stover liquor	Mohagheghi et al. (2014)
8b	ALE	SS3	Xylose utilization and ethanol yields using corn stover hydrolysate	Mohagheghi et al. (2015)
ZM4	NTG mutagenesis	ZM482	Molasses utilization and ethanol productivity	Rogers et al. (1984)
ZM4	NTG mutagenesis	AcR	Ethanol productivity and rate under 20 g/L sodium acetate	Joachimsthal et al. (1998)
ZM4	NTG mutagenesis	ZM401	Cell growth, glucose utilization, and ethanol production under 10.5 g/L acetic acid or 1.0 g/L vanillin	Lee et al. (1982); Zhao et al. (2014)
ZM4	Transposon mutagenesis	ZMT2	Sugar conversion rate to ethanol under 2% NaCl stress	Wang et al. (2016)
ZM4	NTG mutagenesis and ALE	ZMNTG6014	Performance under acetic acid (1.4 or 1.6%)	Wang (2008)
ZM481	NTG mutagenesis and ALE	ZMA-142, ZMA-167	Glucose utilization and ethanol production under 244 mM sodium acetate	Liu et al. (2017)
33C	Transposon mutagenesis and ALE	OEL19, 22, 23, 26, 31	Cell growth under 2-4 g/L furfural	Yang et al. (2014b)
ZM4	gTME (error-prone PCR)	MF1, 2, 3	Glucose utilization under 3 g/L furfural	Tan et al. (2015)

To resolve the limitation of low spontaneous mutation rate using ALE natural selection (Lee et al. 2012), various mutagenesis approaches using chemical, physical, or molecular methods have been developed and employed for microbial strain improvement such as chemical mutagenesis, transposon mutagenesis, genome shuffling, or error-prone PCR. *Z. mobilis* is relatively resistant to mutagenesis, but *N*-methyl-*N'*-nitro-*N*-nitrosoguanidine (NTG) is an effective mutagen (Buchholz and Eveleigh 1990; Typas and Galani 1992). Through mutagenesis with NTG, a salt-tolerant strain ZM482 was isolated, which can tolerate high concentrations of K⁺, Mg²⁺, and Cl⁻ ions (Rogers et al. 1984). Similarly, an acetate-tolerant strain of AcR was also obtained by screening the mutants in the presence of sodium acetate. AcR was capable of efficient ethanol production in the presence of 20 g/L sodium acetate, while the parent strain ZM4 was inhibited completely under the same condition (Joachimsthal et al. 1998). Strain ZM401 is a flocculating mutant of ZM4 generated by NTG mutagenesis as well (Lee et al. 1982). Recent study showed that ZM401 had improved tolerance to inhibitory compounds in the hydrolysate, particularly acetic acid and vanillin, than wild-type strain ZM4, and could be a suitable host for bioethanol production (Zhao et al. 2014). The molecular transposon mutagenesis approach was also applied in *Z. mobilis* (Pappas et al. 1997). A recombinant strain

ZMT2 with improved salt tolerance was achieved via the EZ-Tn5-based transposon insertion mutagenesis, which had higher sugar conversion rate to ethanol under up to 2% NaCl stress than that of wild-type strain ZM4 (Wang et al. 2016).

Forward genetics approaches can also be combined to acquire desired phenotypes effectively. For example, a procedure combining both NTG mutagenesis and ALE approaches was applied to generate and select acetate-tolerant *Z. mobilis* strains, and a desired mutant strain ZMNTG6014 was obtained (Wang 2008). Similar strategy was used to obtain two acetate-tolerant mutants of ZMA-142 and ZMA-167, which exhibited favorable ethanol production under high acetate concentration of 244 mM, while the parental strain ZM481 was completely inhibited by sodium acetate at the concentration above 195 mM (Liu et al. 2017).

Transposon mutagenesis and ALE approaches were also combined to develop robust strains. A transposon-based knockout mutant library of *Z. mobilis* 8b was constructed, and furfural-tolerant mutants were achieved after adaptation using different concentrations of furfural (Yang et al. 2014b). Another "Super Pgap" mutant library was further constructed where the strong native promoter Pgap of *Z. mobilis* was randomly integrated throughout the genome of *Z. mobilis* 33C via an in vitro transposon mutagenesis system. The mutant library

included both insertion knockout mutants and mutants with downstream genes overexpressed if inserted into and replacing original promoters. After continual adaptation with 40% corn stover hydrolysate, five furfural-tolerant mutants (OEL19, OEL22, OEL23, OEL26, and OEL31) were identified with improved furfural- and ethanol-tolerance capability (Yang et al. 2014b).

Robustness improvement by reverse genetics approaches

With the rapid progress to read genetic information by technologies such as next-generation sequencing (NGS) and mass spectrometry, systems biology approaches such as comparative genomics, transcriptomics, proteomics, and metabolomics have been widely applied to understand the underlying molecular stress response mechanisms and to associate genetic elements with improved robustness phenotypes. For example, transcriptomic profiles of *Z. mobilis* wild-type strain ZM4 or its xylose-utilizing derivative 8b in response to furfural, acetate, or phenolic aldehyde inhibitors (4-hydroxybenzaldehyde, syringaldehyde, and vanillin) have been investigated (He et al. 2012; Yang et al. 2014a; Yi et al. 2015). In addition, integrated proteomic and transcriptomic approaches were used to understand the molecular mechanism of an acetate-tolerant strain (Yang et al. 2014c). All these studies demonstrated that multiple-gene regulation is responsive for the inhibitor tolerance in *Z. mobilis* involving in carbohydrate metabolism, DNA replication, recombination and repair, transcriptional regulation, and universal stress responses.

Based on these studies, many candidate genes responsible for the inhibitor tolerance in *Z. mobilis* have been identified, and recombinant strains with enhanced tolerance to lignocellulosic hydrolysates have been constructed by engineering these candidate genes into parental strains. For example, several reductase-encoding genes (ZMO1116, ZMO1696, and ZMO1885) were identified to play key roles in response to phenolic aldehydes through transcriptomics study (Yi et al. 2015). Overexpression of these genes increased the tolerance of *Z. mobilis* ZM4 against hydrolysate inhibitors, especially 4-hydroxybenzaldehyde and vanillin. Transcriptomic studies also led to the identification of a transcriptional regulator *hfq* (ZMO0347), which was differentially regulated in response to various lignocellulosic hydrolysate inhibitors in *Z. mobilis*, and its knockout mutant reduced resistance to acetate, vanillin, furfural, and HMF (Yang et al. 2009b, 2010b).

In addition, genome-resequencing analysis was also applied to identify the underlying genetic changes responsible for the altered phenotypes in mutants generated through forward genetics approaches as discussed

above (Liu et al. 2017; Mohagheghi et al. 2015; Yang et al. 2010a, 2014b). For example, a 1.5-kb deletion in acetate-tolerant strain AcR was identified through comparative genome sequencing, which likely truncated the majority of gene ZMO0117 and partial of the promoter of the *nhaA* gene (ZMO0119) encoding a sodium proton antiporter. Further transcriptomics and genetic studies indicated that the acetate tolerance of AcR was attributed to the overexpression of *nhaA* resulted from the co-transcription of *nhaA* from ZMO0117 (Yang et al. 2010a). Interestingly, a similar result was achieved in another acetate-tolerant mutant ZMA-167 generated through the combination of NTG mutagenesis and ALE (Liu et al. 2017). These two results indicated that overexpression of *nhaA* gene conferred sodium acetate tolerance in *Z. mobilis*.

Another genome-resequencing results of furfural-tolerant mutants confirmed that the improved furfural tolerance of *Z. mobilis* mutants could be due to the overexpression of a histidine kinase encoding gene ZMO1162, the disruption of a Sigma-54 modulation protein encoding gene ZMO0038, and the disruption of 1-deoxy-D-xylulose-5-phosphate synthase encoding genes of ZMO1598 and/or ZMO1234. In addition, the furfural resistance of *Z. mobilis* was also increased in knockout mutants of an efflux pump-encoding operon containing genes of ZMO0282, ZMO0283, and ZMO0285 or in a mutant with the repressor gene ZMO0281 of this efflux pump operon overexpressed (Yang et al. 2014b).

Other inhibitor responsive genes include the alpha subunit of the integration host factor (IHF) encoding gene *himA* (ZMO1122) (Viitanen et al. 2009, 2012; Wang et al. 2016), alcohol dehydrogenase gene ZMO1771 (Wang et al. 2017), TonB-dependent receptor gene ZMO0128 (Yang et al. 2014a), and ZMO1875 with unknown function (Skerker et al. 2013) from *Z. mobilis* ZM4; a functional type II NADH dehydrogenase gene *ndh* (ZZ6_0213) and a terminal cytochrome bd-type ubiquinol oxidase gene *cydAB* (ZZ6_1531 and ZZ6_1532) from *Z. mobilis* ZM6 (Hayashi et al. 2015); as well as a regulatory protein encoding gene *irrE* from *Escherichia coli* (Zhang et al. 2010) and a formate dehydrogenase encoding gene *fdh* from *Saccharomyces cerevisiae* (Dong et al. 2013).

The strategy of global transcription machinery engineering (gTME) has also been applied in *Z. mobilis* to improve inhibitor tolerance (Alper and Stephanopoulos 2007; Tan et al. 2015). For example, the global transcription factor RpoD protein, the main sigma factor σ^{70} in *Z. mobilis*, was subjected to random mutagenesis through error-prone PCR with three mutants (ZM4-MF1, ZM4-MF2, and ZM4-MF3) exhibiting enhanced furfural tolerance selected (Tan et al. 2015). This approach provides

an alternative route for identifying transcription factor mutants with improved tolerance against various stresses, and will be an effective strategy for improving other similar complex phenotypes involved in multiple genes in the future.

Conclusions and perspectives

Zymomonas mobilis has been developed as an effective model for biofuel and biochemical production from lignocellulosic materials. However, microbial fermentation is still commonly affected by the presence of toxic inhibitors in the hydrolysate, which severely impeded its industrial application (Franden et al. 2013; Yi et al. 2015). Besides the lack of complete information on inhibitory compounds in the hydrolysates due to the detection limitation of current techniques, little is known on potential additional/synergetic effects of these inhibitory compounds on cellular metabolism. In addition, although recombinant strains capable of co-fermentation of pentose and hexose sugars have been achieved (Deanda et al. 1996; Dunn and Rao 2014; Yanase et al. 2012; Zhang and Eddy 1995), all these strains were sensitive to inhibitor stress, especially for the xylose utilization (Kim et al. 2000; Yang et al. 2014a). Pentose sugar xylose actually affects cellular metabolism more significantly than hydrolysate inhibitors for *Z. mobilis*, and the co-fermentation of xylose and glucose in the presence of inhibitor remains the key barrier for economic lignocellulosic biofuel production.

Numerous approaches have been developed to circumvent or alleviate the hydrolysate toxicity on microbial biocatalysts. One strategy is to improve pretreatment and hydrolysis processes using less severe conditions to increase sugar contents while reducing the inhibitor concentrations. Recently, a highly efficient deacetylation and mechanical refining (DMR) process has been developed resulting in low toxicity and high concentration of mixed sugars that are superior for ethanol production by *Z. mobilis* (Chen et al. 2012, 2016). Another strategy is to develop robust *Z. mobilis* strains with enhanced ethanol productivity in the presence of hydrolysate inhibitors.

As discussed above, different forward genetics strategies such as classical ALE, chemical, and transposon mutagenesis have been applied so far in *Z. mobilis* for inhibitor tolerance improvement. More recently, a novel mutagenesis approach, the atmosphere and room temperature plasma (ARTP) mutation, developed by Tsinghua University, is becoming increasingly popular owing to its rapid mutation, highly diverse mutants, as well as simple and safe operation (Zhang et al. 2014, 2015). ARTP has been demonstrated as a powerful tool for phenotype improvement in many different strains (Cao et al. 2017b; Chen 2016; Jiang et al. 2014). We have applied this

method in *Z. mobilis* to improve its tolerance against low pH and high glucose concentration with positive preliminary results.

Moreover, systems biology approaches, as the reverse genetics strategies, should be continuously carried out and cross-compared to provide a complete understanding of the inhibitor tolerance mechanism of *Z. mobilis*, and more biological parts related to inhibitor tolerance should be continuously identified and characterized for robust strain development. For example, small RNAs (sRNAs) and 5'UTR in *Z. mobilis* have been studied recently by transcriptomics and bioinformatics approaches, and the result suggested that sRNAs potentially can be developed as novel biological parts to improve the tolerance against various inhibitors in *Z. mobilis* (Cho et al. 2014, 2017).

Considering that even simple modification in genome may switch cellular metabolism or redox balance and thereby decrease the overall yield of the system, sophisticated computational models should be developed to guide future genetic or metabolic engineering efforts in *Z. mobilis* (Kalnenieks et al. 2014; Widiastuti et al. 2011; Yadav et al. 2012). In addition, with the rapid development of synthetic biology tools and strategies especially the recent breakthrough on yeast genome synthesis (Wu et al. 2017; Xie et al. 2017; Zhang et al. 2017), it is advantageous and practical to develop ZM4 as a chassis microorganism through both genome minimization and genome synthesis approaches considering its excellent industrial features, small genome size of 2.06 Mb, and fascinating unique physiology. The synthetic minimal *Z. mobilis* chassis can facilitate the understanding of functional and regulatory biological parts and their potential synergetic effects as well as the underlying mechanisms against inhibitor tolerance for the development of robust industrial chassis platforms for economic bioproducts. Finally, sophisticated and efficient tools for genome editing need to be developed instantaneously. For example, although CRISPR/Cas system has been investigated in *Z. mobilis* recently (Cao et al. 2017a; Dong et al. 2016), more efficient strategies are needed for efficient recreation of SNPs for genetics studies to identify the association of SNPs with improved phenotypes in tolerant mutants.

Another major bottleneck impeding strain-engineering efforts are the lack of high-throughput screening and characterization methods to correlate genetic change(s) acquired through forward and reverse genetics approaches with microbial physiology and bioproduction parameters of titer, rate, and productivity. Although high-throughput approaches such as Bioscreen C have been applied in *Z. mobilis*, cutting-edge versatile high-throughput methods should be continuously developed and employed to accelerate the strain characterization

such as microfluidics and microfluidics-based advanced microscopy techniques (Gan et al. 2011; Madren et al. 2012).

In summary, the application of various advanced technological approaches will be further implemented with a promising future in developing more robust *Z. mobilis* strains for efficient biofuels and biochemicals production from lignocellulosic biomass.

Abbreviations

ED pathway: Entner–Doudoroff pathway; GRAS: generally regarded as safe; ALE: adaptive laboratory evolution; ILs: ionic liquids; STEX: steaming or steam explosion; AFEX: ammonia fiber explosion; LHW: liquid hot water; HMF: 5-hydroxymethyl-2-furaldehyde; HPLC: high-performance liquid chromatography; GC: gas chromatography; GC–MS: gas chromatography–mass spectrometer; LC–MS: liquid chromatography–mass spectrometer; ICP–MS: inductively coupled plasma mass spectrometer; ICP–OES: inductively coupled plasma optical emission spectrometry; NMR: nuclear magnetic resonance; PCR: polymerase chain reaction; NTG: *N*-methyl-*N'*-nitro-*N*-nitrosoguanidine; NGS: next-generation sequencing; sRNAs: small RNAs; DMR: deacetylation and mechanical refining.

Authors' contributions

SY conceived the concept with inputs from XW and YY. YY, HM, TY, BG, and MQ prepared and wrote the manuscript. SY revised the manuscript with inputs from QH, SC, and XW. All authors read and approved the final manuscript.

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Competing interests

The authors declare that they have no competing interests.

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